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(54) **PROCESS FOR THE PREPARATION OF LINEAR LOW DENSITY POLYETHYLENE.**(30) Priority: **31.07.91 IT MI912142**(43) Date of publication of application:
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Description

The present invention relates to a process for the preparation of linear low density polyethylene (LLDPE) endowed with improved processability by gas phase polymerization of the monomers, in two or more fluidized bed or mechanically stirred bed reactors, wherein, whatever the order, in one of the reactors mixtures of ethylene and an alpha-olefin $\text{CH}_2 = \text{CHR}$ (R = alkyl having 1-10 carbon atoms) are polymerized to yield LLDPE and in another reactor mixtures of propylene and an alpha-olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having 2-18 carbon atoms, are polymerized, using the same catalyst in both reactors.

LLDPE has a variety of applications, but it is particularly employed in the preparation of films, because LLDPE films are endowed with improved mechanical and optical properties compared to films of LDPE.

The production of LLDPE films, however, shows some difficulties, mainly due to the fact that the polymer in the melted state has an insufficiently high melt strength, while its viscosity in the melted state is rather high.

In order to keep the productivity unaltered, it is necessary to modify the film extruders, for instance by widening the slit or increasing the temperature of the extruder head.

These modifications cause difficulties in the cooling of the bubble being blown at the extruder outlet and dishomogeneity in the film thickness.

In addition to these drawbacks, the hot welding of LLDPE films shows poor resistance to heat.

In order to overcome the shortcomings above, it was proposed to use blends of LLDPE with a semicrystalline copolymer of propylene with an alpha-olefin $\text{CH}_2 = \text{CHR}'$ where R' is an alkyl radical having 2-10 carbon atoms, in particular 1-butene (U.S. Patent 4,871,813).

The copolymer contains from 7 to 40% by weight of alpha-olefin, has a fusion enthalpy lower than 75 J/g and is added in an amount of from 1 to 25% by weight.

The LLDPE-copolymer blend is prepared by mixing in the melted state the components pre-mixed in the solid state (in the form of powder or granules).

Mixing of the components in the solid state and feeding of such mixture directly into the extruder to mold the finished article is also contemplated.

The LLDPE is obtained by conventional polymerization methods, whereas the propylene-alpha olefin copolymer is prepared separately, employing stereospecific catalysts capable of yielding a semicrystalline copolymer having a fusion enthalpy not higher than 75 J/g.

The preparation of the above blends requires two separate polymerization lines for producing the two polymer components and then a blending step for mixing the components in the melt in an extruder. Blending of polymers in the melt is a high energy - consuming operation.

It has now been found that it is possible to produce blends of LLDPE and a propylene-alpha olefin $\text{CH}_2 = \text{CHR}'$ copolymer endowed with improved processability and capable of forming films exhibiting good mechanical and optical properties directly in polymerization, using at least two reactors in series, wherein, whatever the order, in one of the reactors the LLDPE and in the other the propylene-alpha olefin copolymer are synthesized and wherein in both reactors the same catalyst is employed.

The use of the same catalyst in the various reactors in series has the advantage of utilizing a single production line instead of two, as well as growing the polymer blend onto each catalyst particle, thus obtaining a composition in which the components are homogeneously mixed in the solid state, with no need of the pelletization step which is necessary when the components are prepared by separate processes.

Therefore, the polymer can be directly fed into the film extruders, thereby attaining a higher film production rate and a lower energy consumption. In fact, the non-pelletized granules, not having been subjected to the melting-solidification process of the pelletization step, have lower crystallinity and higher melt index.

Moreover, the homogenization at the level of each single particle achievable by the process of the present invention has beneficial effects on the properties of the film.

The process of the invention comprises the following steps:

- a) pre-contact of the catalyst components in the substantial absence of polymerizable olefins (the olefins should not be present in such a quantity as to produce more than 1 g polymer/g of solid catalyst component) operating in such a way as to obtain a stereospecific catalyst capable of yielding during the polymerization step
- c2) a copolymer having an insolubility in xylene at 25 °C of at least 80%;
- b) pre-polymerization, using the catalyst obtained in step a), of propylene or mixtures thereof with ethylene and/or alpha-olefins $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 2 to 10 carbon atoms, such as butene-1, hexene-1, 4-methyl-pentene-1, in such conditions as to obtain a polymer having an insolubility in xylene at 25 °C higher than 60%, in an amount of from 1 to 1000 g per g of solid catalyst component;

c) polymerization of the monomers in gas phase, performed in two or more fluidized bed or mechanically stirred bed reactors in series, wherein, whatever the order:

c1) in one of the reactors a mixture of ethylene and an alpha-olefin $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, is polymerized to obtain an ethylene-alpha olefin copolymer containing up to 20% by moles of alpha-olefin, and

c2) in another reactor, after removing the unreacted monomers coming from the reactor c1) if c1) is the first reactor, a mixture of propylene and an alpha-olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having from 2 to 10 carbon atoms, is polymerized to yield a copolymer containing from 5 to 40% by weight of the alpha olefin, in an amount of 5-30% by weight with respect to the total weight of the polymer obtained in c1) and c2);

and wherein the prepolymer-catalyst system obtained in b) is fed to the reactor in c1) and the polymer-catalyst system obtained in c1) to the reactor in c2). In case the first reactor is used in c2), the unreacted monomers coming from c2) are removed before feeding the reactor in c1) with the polymer-catalyst system obtained in c2).

Preferably, for an efficient control of the gas phase reaction, an alkane having 3-5 carbon atoms, preferably propane, is kept in the reaction gas, in particular in the first reactor where the catalyst reactivity is higher, in a concentration of from 20 to 90% by moles based on the total gas.

Preferably, the copolymer formed in c2) contains 10-15% by weight of the alpha-olefin and forms 15-25% of the total weight of the polymer in c1) and c2).

Surprisingly and unexpectedly the pre-forming of the catalyst, the pre-polymerization treatment with propylene and the presence of an alkane in the gas phase in the molar concentration indicated above, allow to control the polymerization process in the gas phase without the drawbacks usually encountered in the processes of the prior art, drawbacks which are essentially due to the low heat transfer capability of the gas phase and to the formation of electrostatic charges, which determine the tendency of the catalyst and the polymer particles to adhere to the reactor walls.

The catalyst employed in the process of the invention furthermore allows the polymer blend to grow onto each single particle of the solid catalyst component, so obtaining a good homogenization of the polymer blend.

The catalyst components employed in step a) comprise:

1) A solid component comprising a titanium compound containing at least one titanium-halogen bond supported on a magnesium halide in active form.

The solid component also contains an electron-donor compound (internal donor) when the catalyst itself is not sufficiently stereospecific for producing in step c2) propylene copolymers having the insolubility characteristics reported in c2).

As known, the stereospecificity of the catalysts supported on magnesium dihalide increases when using an internal donor.

As a general rule, the internal donor is always used in order to obtain catalysts capable of yielding in step c2) propylene-alpha olefin $\text{CH}_2 = \text{CHR}'$ copolymers having an insolubility in xylene higher than 80% and preferably comprised between 85-94%.

2) An alkyl aluminum compound.

3) Optionally an electron-donor compound (external donor) of the same or of a different type with respect to the electron-donor present in the solid component 1).

The external donor is used to confer to the catalyst the required high stereospecificity. However, when particular diethers are employed as internal donors, such as those described in the European Patent Application A-344755, the catalyst stereospecificity is sufficiently high and no external donor is required.

The catalyst formed in step a) is fed continuously or discontinuously into step b).

Step b) can be carried out in liquid or gas phase. Preferably, step b) is carried out in the liquid phase, using as a liquid medium the propylene itself or a hydrocarbon solvent such as n-hexane, n-heptane, cyclohexane or an alkane having a low boiling point such as propane, butane (kept in the liquid state in the conditions employed in b)).

The propylene pre-polymerization in step b) is carried out at a temperature comprised in the range of from 0° to 80°C, preferably from 5° to 50°C.

Propylene or the mixtures of propylene with ethylene and/or other alpha olefins, such as butene-1, hexene-1, 4-methyl pentene-1, are polymerized to yield polymers having an insolubility in xylene higher than 60%. The prepolymer yield ranges from 1 g to 1000 g of polymer per g of solid catalyst component, preferably from 5 g to 500 g of polymer per g of solid catalyst component.

Step b) can be performed continuously or discontinuously. In the former case, suitable means are employed for removing the unreacted propylene prior to feeding the prepolymer-catalyst system of step b)

to the gas phase reactor.

The gas phase polymerization of step c) is performed according to known techniques operating in two or more fluidized bed or mechanically stirred bed reactors connected in series.

The monomers are fed into the two reactors in such a ratio as to yield a copolymer having the desired composition.

As indicated above, the unreacted monomers are removed prior to feeding the reaction mixture of the first reactor into the second reactor.

The process is carried out at a temperature lower than the synthesis temperature of the polymer. Generally the temperature is comprised between 50° and 120°C and preferably between 60° and 100°C.

The total pressure is comprised between 1.5 and 3 MPa.

As indicated above, it is immaterial whether the ethylene-alpha olefin mixture is polymerized first to form the LLDPE copolymer or the propylene-alpha olefin $\text{CH}_2 = \text{CHR}'$ mixture is polymerized first to form the corresponding copolymer.

However, synthesizing the propylene-alpha olefin copolymer in the first reactor is preferred, in order to obtain a polymer endowed with better flowability and a higher bulk density.

The propylene-alpha olefin copolymer is characterized by a fusion enthalpy (measure in accordance with the DSC method described in U.S. Patent 4,871,013) higher than 70 J/g, preferably comprised between 75 and 95 J/g, and by an isotactic index (determined by measuring the copolymer fraction which is insoluble in xylene at 25 °C) higher than 80 and generally comprised between 85 and 94.

Said DSC method consists in recording the enthalpy graph of a 5 mg sample of a copolymer by heating at a speed of 16°C. per minute up to 200°C., the sample having been previously subjected to a thermal treatment formed by heating at a speed of 16°C. per minute up to 200°C., followed by maintenance of such temperature for 20 minutes and cooling at a speed of 16°C. per minute down to 50°C.; the surface of the endothermic peak recorded during the heating is proportional to the melting enthalpy: the DSC analysis therefore enables the melting enthalpy of the copolymer to be measured, corresponding to the quantity required to melt 1 gramme of such copolymer.

Surprisingly, and in contrast with the characteristics of the propylene-alpha olefin copolymers used in the prior art, the process of the present invention allows to obtain LLDPE polymers endowed with good processability even though the crystallinity and isotacticity of the copolymer used are high.

As indicated above, the gas phase present in the various reactors preferably contains a C₃-C₅ alkane in a molar amount of from 20 to 90% with respect to the total gases. Examples of suitable alkanes are propane, butane, isobutane, n-pentane, isopentane, cyclopropane, cyclobutane. Propane is the preferred alkane.

The alkane is fed into the first reactor with the monomer mixture or separately and it is recycled with the recycle gas, i.e. with the portion of the gas which does not react in the bed and is removed from the polymerization zone, preferably by conveying it into a zone above the bed where the velocity is reduced and the particles entrained in the gas can again fall into the bed.

The recycle gas is then compressed and passed through a heat exchanger, where the heat of reaction is removed, before being recycled to the bed. See, for instance, U.S. Patents 3,298,792 and 4,518,750 for a description of the gas phase technology.

It is surprising and completely unexpected that the alkanes allow a very good control of the gas phase reaction whereas using an inert gas such as nitrogen is ineffective. In fact, the use of nitrogen does not prevent the formation of large polymer aggregates ("chunks"), which necessarily cause stopping of the operation of the plant.

According to a preferred embodiment, the alkane concentration in the first reactor is kept higher than that in the second (or subsequent) reactor.

Generally, the alkane is circulated through both reactors.

To achieve a complete fluidization, the recycle gas and, if preferred, a part or all of the make-up gas are reintroduced into the reactor at a point under the bed. A gas distribution plate, placed above the point of return, allows an effective distribution of the gas and furthermore acts as a support for the polymer bed when the gas flow is stopped.

Hydrogen can be used as chain transfer agent to control the molecular weight of the polymer.

A typical simplified scheme of the process is shown in the attached Figure 1. Reference numeral 1 indicates the apparatus where the catalyst components are pre-contacted. The loop reactor 2 is the pre-polymerization reactor. The gas phase reactors are indicated with 4 and 6, the solid-fluid separators with 3, 5 and 7. The catalyst components and the diluting agent (propane) are fed into the pre-contact reactor 1, as shown by arrows A. The pre-contacted catalyst is fed into the loop reactor 2 as shown by arrows B; propylene is fed into said loop reactor as shown by arrow E. The prepolymer-catalyst system is fed into the

separator 3 and from the latter into the gas phase reactor 4, where, in the gas recycle line, propylene, the alpha olefin $\text{CH}_2 = \text{CHR}'$, hydrogen and propane are fed, as shown by arrow C. The polymer which leaves the reactor 4, after passing through the separator 5, is introduced into the reactor 6, where ethylene, the alpha olefin $\text{CH}_2 = \text{CHR}$, hydrogen and propane are fed, as shown by arrow D. The polymer in the form of spherical granules is discharged from the reactor 6 into the separator 7.

The active magnesium dihalides used as support for Ziegler-Natta catalysts are widely described in patent literature. The use of such dihalides is described for the first time in the U.S. Patents 4,298,718 and 4,495,338.

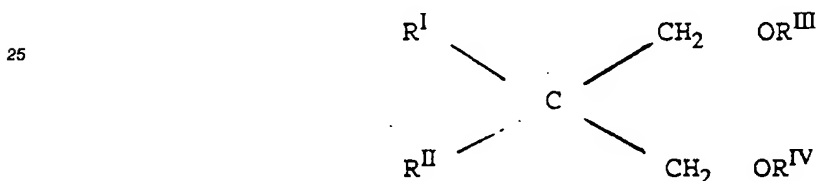
The magnesium dihalides which form the support for the catalyst components employed in the process of the present invention are characterized by X-ray spectra wherein the most intense diffraction line appearing in the spectrum of the non-active halide has a lowered intensity and is substituted by a halo which maximum intensity is shifted toward lower angles with respect to the most intense line.

In the most active forms of the magnesium dihalides, the most intense line is no longer present and is substituted by a halo with the maximum intensity shifted as described above.

The titanium compounds suitable for the preparation of the solid catalyst component comprise the titanium halides, such as TiCl_4 , which is preferred, and TiCl_3 , and the haloalcoholates, such as trichlorophenoxy titanium and trichlorobutoxy titanium.

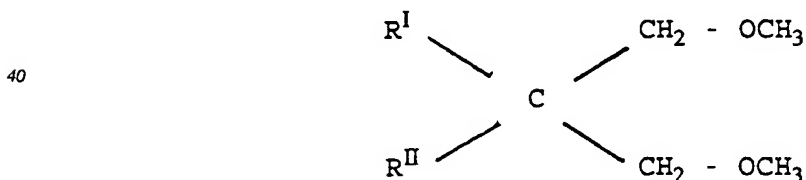
The titanium compound can be used as a mixture with other transition metal compounds, such as vanadium, zirconium and hafnium.

Suitable internal electron-donors comprise ethers, esters, amines, ketones and diethers of the general formula:



wherein R^{I} and R^{II} , equal to or different from each other, are alkyl, cycloalkyl and aryl radicals having from 1 to 18 carbon atoms, and R^{III} and R^{IV} , equal to or different from each other, are alkyl radicals having from 1 to 4 carbon atoms.

The preferred compounds are the alkyl, cycloalkyl and aryl esters of polycarboxylic acids such as phthalic and maleic acid and diethers of the formula:



wherein R^{I} and R^{II} are defined as above.

Examples of such compounds are: di-n-butyl-phthalate, di-isobutyl-phthalate, di-n-octyl-phthalate, 2-methyl-2-isopropyl-1,3-dimethoxy-propane, 2-methyl-2-isobutyl-1,3-dimethoxy-propane, 2,2-di-isobutyl-1,3-dimethoxypropane and 2-isopropyl-2-isopentyl-1,3-dimethoxy-propane.

The internal donor is generally present in molar ratios of from 1:8 to 1:14 with respect to Mg. The titanium compound, expressed as Ti, is present in amounts of from 0.5 to 10% by weight.

The solid catalyst components can be prepared according to the methods described in the U.S. Patents 4,748,221 and 4,803,251.

If the stereospecificity of the obtained catalyst is insufficient for the purposes of the present invention, it can be easily modified according to the well known techniques described above.

Using the catalysts prepared from the catalyst components described in the European Patent Application EP-A-344,755, it is possible to obtain, with high specific activities (generally from 10 to 100 Kg/h/g of solid catalyst component), spherically shaped polymers with an average diameter of from 300 to 5000 μm

(microns), endowed with high bulk density and flowability.

In particular, in the European Application indicated above the catalyst components are prepared from spherulized adducts $\text{MgCl}_2 \cdot n \text{ ROH}$ (R' is an alkyl or cycloalkyl radical having 2-10 carbon atoms and n is a number from 3.5 to 2.5), from which the alcohol is partially removed by heating at increasing
 5 temperatures of from 50 °C to 100 °C.

In the formula above n is a number from 3.5 to 2.5; by heating, n is lowered to values of from 2.5 to 1 or lower.

The spherulized and partially de-alcoholated product is reacted with an excess of TiCl_4 at temperatures of from 80 ° to 135 °C; the excess of TiCl_4 is removed for instance by hot filtration.

10 The treatment with TiCl_4 is usually repeated and the solid from which the unreacted TiCl_4 is removed is then washed with an inert hydrocarbon until the reaction of chlorine ions disappears.

The reaction with TiCl_4 is carried out in the presence of an electron-donor compound, selected in particular from the alkyl esters of the phthalic acid, such as di-n-butyl-phthalate, di-isobutyl-phthalate, di-n-octyl-phthalate, and the diethers having the general formula above.

15 The electron-donor compound can also be reacted with the adduct, before the reaction with the titanium compound.

The alkyl aluminum compound employed as co-catalyst is selected from the trialkyl aluminum compounds, such as Al-triethyl, Al-triisobutyl, Al-tri-n-butyl, Al-tri-n-octyl. Mixtures of trialkyl aluminum compounds with Al-alkylhalides or Al-alkyl-sesquihalides, such as AlEt_2Cl and $\text{Al}_2\text{Et}_3\text{Cl}_3$, can also be
 20 employed.

The Al/Ti ratio in the catalyst formed in step a) is greater than 1 and is generally comprised between 20 and 800.

The external donor can be the same or different from the electron-donor compound present as internal donor.

25 The molar ratio alkyl aluminum compound/external donor is generally comprised between 2 and 30.

When the internal donor is an ester of a polycarboxylic acid, particularly a phthalate, for instance isobutylphthalate or n-octylphthalate, the external donor is preferably selected from the silicon compounds of the formula $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ or $\text{R}_1\text{Si}(\text{OR})_3$, where R_1 and R_2 are alkyl, cycloalkyl or aryl radicals having from 1 to 18 carbon atoms and R is an alkyl radical having 1-6 carbon atoms. Examples of said silanes are methyl-
 30 cyclohexyl-dimethoxy silane, diphenyl-dimethoxy silane, methyl-t-butyl-dimethoxy silane and triphenyl methoxysilane.

The diethers of the general formula reported above can also be conveniently used as external donors.

The solubility in xylene of the propylene polymer prepared in step b) and also of the propylene-alpha olefin copolymer is determined by dissolving 2 g of polymer in 250 ml of xylene at 135 °C and stirring the
 35 system. After 20 minutes, the solution is cooled down to 25 °C. After 30 minutes the precipitated material is filtered; the solution is evaporated in a nitrogen flow and the residue is dried at 80 °C.

In this manner the percentage of polymer in xylene at room temperature and the percentage of insoluble polymer are calculated.

The following examples are given to better illustrate the invention and cannot be construed as limitative
 40 of its scope. Unless otherwise indicated, all the data are expressed by weight.

General procedure

The solid catalyst component employed in the examples is prepared as follows:

45 28.4 g of MgCl_2 , 49.5 g of anhydrous ethanol, 10 ml of vaseline oil ROL OB/30 and 100 ml of silicone oil having a viscosity of 350 cs are introduced, in an inert atmosphere, into a reactor equipped with a stirrer and heated to 120 °C, until MgCl_2 is dissolved. The hot reaction mixture is then transferred into a 1,500 ml vessel, equipped with a stirrer Ultra Turrax T-45 N and containing 150 ml of vaseline oil and 150 ml of silicone oil. The temperature is kept at 120 °C while stirring for 3 minutes at 3,000 r.p.m. The mixture is
 50 then discharged into a 2 liter vessel equipped with a stirrer and containing 1,000 ml of anhydrous n-heptane cooled to 0 °C. The mixture is stirred at a speed of 6 meters per second for about 20 minutes, keeping the temperature at 0 °C. The so obtained particles are recovered by filtration, washed with 500 ml of n-hexane and gradually heated, increasing the temperature from 50 °C to 100 °C for a time sufficient to reduce the alcohol content from 3 moles to the molar content indicated in the examples.

55 The adduct (25 g), containing the alcohol in the amounts indicated in the examples, is transferred into a reactor equipped with a stirrer and containing 625 ml of TiCl_4 at 0 °C, under stirring. The reactor is then heated to 100 °C for one hour. When the temperature is 40 °C, di-isobutylphthalate is added in such an amount that the Mg/phthalate molar ratio is 8.

The reactor contents are then heated to 100°C for two hours and then the solid separates by sedimentation.

The hot liquid is removed by a siphon. 500 ml of TiCl_4 are added and the mixture is heated to 120°C for an hour under stirring. Stirring is stopped and the solid separates by sedimentation. The hot liquid is removed by a siphon. The solid is washed with portions of n-hexane at 60°C and then at room temperature.

Example 1.

An apparatus is utilized which operates in continuous and comprises a reactor in which the catalyst components are mixed to form the catalyst, a loop reactor receiving the catalyst formed in the previous step and being fed with liquid propylene and propane, and two fluidized bed reactors connected in series, the first reactor receiving the pre-polymer formed in the preceding step and discharging the polymer into the second reactor after removal of the unreacted monomers.

The process is carried out by feeding a solid catalyst component, prepared according to the general method reported above using a MgCl_2 /ethanol adduct containing 35% by weight of alcohol, a solution of triethyl aluminum (TEAL) in n-hexane and methyl-cyclohexyl-dimethoxysilane as electron-donor in such an amount that the TEAL/silane ratio is 4 by weight and the TEAL/Ti ratio is 120 by moles, into the pre-contact reactor kept at the constant temperature of 20°C. Into the same reactor propane is also fed as inert medium. The residence time is about 8.8 minutes.

The product discharged from the reactor is then fed into a loop pre-polymerization reactor kept at 50°C. The residence time in the loop reactor is about 80 minutes.

The first reactor receiving the pre-polymer produced in the preceding step operates at 60°C and at a reaction pressure of 1.8 MPa.

The average residence time of the polymer forming inside the reactor is about 80 minutes.

The reaction monomers and the gases fed into the reactor are the following:

- propylene and butene;
- hydrogen as molecular weight regulator;
- propane.

The first reactor discharges into a gas-solid separation system which removes the undesired monomer (propylene) before feeding the polymer to the second polymerization step.

Main operating conditions

Pre-contact step

- temperature (°C)	= 20
- residence time (min.)	= 8.8

Pre-polymerization step

- temperature (°C)	= 50
- residence time (min.)	= 80

First gas phase reactor

5	- temperature (°C)	= 60
	- pressure (MPa)	= 1.8
	- residence time (min)	= 68
	- propylene (mole%)	= 4.8
	- butene-1 (mole%)	= 1.2
10	- hydrogen (mole%)	= 0.6
	- propane (mole%)	= 89
	- % polymerization	= 11
	- bonded butene (wt%)	= 9.8
15	- MIL (230 °C) (g/10 min)	= 21

Second gas phase reactor

20	- temperature (°C)	= 90
	- pressure (MPa)	= 1.75
	- residence time (min)	= 76
	- butene-1 (mole %)	= 8.6
25	- ethylene (mole %)	= 34
	- hydrogen (mole %)	= 9.2
	- propane (mole %)	= 44
	- % polymerization	= 89
	- bonded butene (wt %) (final)	= 7
30	- MIE (190 °C, 2.16 Kg) (final) (g/10 min)	= 1.1
	- F/E (21.6 Kg/2.16 Kg) (final)	= 35
	- density (final) (g/cm ³)	= 0.916

35 Example 2

The same apparatus is used as in Example 1.

The process is carried out by feeding the catalyst components into the pre-contact reactor, kept at a constant temperature of 0 °C with a residence time of 9.5 min.

40 The product discharged from the reactor is then fed into a loop pre-polymerization reactor, wherein a certain amount of liquid propylene and propane is also fed (as inert medium).

The residence time in the pre-polymerization reactor is about 80 minutes and the temperature is kept at 50 °C.

45 The first reactor receiving the pre-polymer formed in the preceding step operates at 60 °C and at a reaction pressure of 1.8 MPa.

The reaction monomers and the gases fed into the reactor are the following:

- ethylene;
- hydrogen as molecular weight regulator;
- propane.

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Main operating conditions

Pre-contact step

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- temperature (°C)	= 0
- residence time (min)	= 9.5

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Pre-polymerization step

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- temperature (°C)	= 50
- residence time (min)	= 80

First gas phase reactor

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- temperature (°C)	= 60
- pressure (MPa)	= 1.8
- residence time (min)	= 45
- propylene (mole %)	= 15
- butene-1 (mole %)	= 3.5
- hydrogen (mole %)	= 0.5
- propane (mole %)	= 80
- % polymerization	= 24
- bonded butene (wt %)	= 11.2
- MIL (230°C) (g/10 min)	= 6.1

Second gas phase reactor

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- temperature (°C)	= 90
- pressure (MPa)	= 1.75
- residence time (min)	= 83
- butene-1 (mole %)	= 4.8
- ethylene (mole %)	= 23
- hydrogen (mole %)	= 4.2
- propane (mole %)	= 68
- % polymerization	= 76
- bonded butene (wt %) (final)	= 7.5
- MIE (190°C, 2.16 Kg) (final) (g/10 min)	= 1.14
- F/E (21.6/2.16) (final)	= 50
- density (final) (g/cc)	= 0.915

The particle size distribution of the polymers obtained in Examples 1 and 2 are reported in Table 1.

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Table 1

SIZE DISTRIBUTION	Units	Example 1	Example 2
over 2,800 μm	wt %	0.5	1.0
over 2,000 μm	wt %	18.3	18.0
over 1,400 μm	wt %	45.0	41.6
over 1,000 μm	wt %	29.2	30.3
over 710 μm	wt %	5.0	7.5
over 500 μm	wt %	0.6	0.8
over 300 μm	wt %	0.3	0.4
over 180 μm	wt %	0.2	0.3
over 106 μm	wt %	0.1	0.1
Residue	wt %	---	---
BULK DENSITY			
Poured	g/cm^3	0.398	0.425
Tamped	g/cm^3	0.425	0.464
FLOWABILITY	s	10.0	9.0

Claims

- Process for the preparation of ethylene polymers endowed with improved processability by polymerization of ethylene with olefins $\text{CH}_2 = \text{CHR}$, where R is an alkyl having 1-10 carbon atoms, by means of catalysts comprising the product obtained by reacting an alkyl aluminum compound with a solid component comprising a titanium halide or halo-alcoholate and optionally an electron-donor compound supported on a magnesium halide in active form, which process comprises the following steps:
 - pre-contact of the catalyst-forming components in the substantial absence of polymerizable olefins (the olefins should not be present in such a quantity as to produce more than 1 g polymer/g of catalyst component) to form a stereospecific catalyst capable of yielding during the polymerization of the mixture of propylene and alpha olefins in step c2) a copolymer having an insolubility in xylene at 25 °C of at least 80%;
 - pre-polymerization, using the catalyst obtained in step a), of propylene or mixtures thereof with ethylene and/or alpha-olefins $\text{CH}_2 = \text{CHR}$, where R is an alkyl having from 2 to 10 carbon atoms, in such conditions as to obtain a polymer having an insolubility in xylene at 25 °C higher than 60%, in an amount of from 1 to 1000 g per g of solid catalyst component;
 - polymerization of the monomers in the gas phase, operating in two or more fluidized bed or mechanically stirred bed reactors in series, wherein, whatever the order:
 - in one of the reactors a mixture of ethylene and an alpha-olefin $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, is polymerized to obtain a copolymer of ethylene with said alpha olefin copolymer containing up to 20% by moles of the alpha-olefin; and,
 - in another reactor, after removing the unreacted monomers coming from the reactor c1) if c1) is the first reactor, a mixture of propylene and an alpha-olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having from 2 to 10 carbon atoms, is polymerized to yield a copolymer containing from 5 to 40% by weight of the alpha olefin, in an amount of 5-30% by weight with respect to the total weight of the polymer obtained in c1) and c2);
 and wherein the prepolymer-catalyst system obtained in b) is fed into the reactor in c1) and the polymer-catalyst system obtained in c1) is fed to the reactor in c2), and in case the first reactor is used in c2), the unreacted monomers coming from c2) are removed before feeding the reactor in c1) with the polymer catalyst system obtained in c2).

2. Process according to claim 1, wherein the copolymer formed in c2) contains 10-15% by weight of the alpha-olefin and forms 15-25% of the total weight of the polymer obtained in c1) and c2).
3. Process according to claims 1 and 2, wherein the copolymer formed in c2) is a propylene-butene
5 copolymer having an insolubility in xylene at 25 °C higher than 85%.
4. Process according to claim 1, wherein in step c) firstly the propylene-alpha olefin $\text{CH}_2 = \text{CHR}'$ mixture of c2) is polymerized and thereafter the ethylene-alpha olefin mixture of c1) is polymerized.
- 10 5. Process according to claim 1, wherein the catalyst is obtained by reaction of an alkyl aluminum compound, an electron-donor compound and the solid component.
6. Process according to claim 5, wherein the electron-donor compound is a silane of formula $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ or $\text{R}_1\text{Si}(\text{OR})_3$ wherein R_1 and R_2 , the same or different, are alkyl, cycloalkyl or aryl radicals with 1-18
15 carbon atoms and R is an alkyl radical with 1-6 carbon atoms.
7. Process according to claim 1, wherein in the reaction gases an alkane having 3-5 carbon atoms is kept in a concentration of from 20 to 90% by moles on the total gases.
- 20 8. Process according to claim 7, wherein the alkane is propane.
9. Process according to claim 1, wherein the solid catalyst component is obtained from spherulized adducts $\text{MgCl}_2 \cdot n \text{R}'\text{OH}$, where R' is an alkyl or a cycloalkyl radical having 1-10 carbon atoms and n is a number from 3.5 to 2.5, from which the alcohol is partially removed up to values for n of from 2.5
25 to 0.5.
10. Ethylene polymers in the form of particles, which particles comprise a mixture of a linear copolymer of ethylene with an alpha olefin $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, containing up to 20% by moles of the alpha olefin, in an amount of from 70 to 95% by weight with
30 respect to the total weight of the mixture, and a copolymer of propylene with an alpha olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having 2-10 carbon atoms, containing from 5 to 30% by weight of the alpha olefin, in an amount of from 5 to 30% by weight with respect to the total weight of the mixture, said copolymer having an insolubility in xylene at 25 °C of at least 80% and a fusion enthalpy of more than 70 J/g.
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11. Pelletized compositions obtained from the polymer particles according to claim 10.
12. Films obtainable from the polymers according to claims 10 and 11.

40 Patentansprüche

1. Verfahren zur Herstellung von mit verbesserter Verarbeitbarkeit ausgestatteten Ethylenpolymeren durch Polymerisation von Ethylen mit Olefinen $\text{CH}_2 = \text{CHR}$, worin R Alkyl mit 1-10 Kohlenstoffatomen darstellt, mit Hilfe von Katalysatoren, umfassend das Produkt, erhalten durch Umsetzen einer Alkylaluminiumver-
45 bindung mit einer festen Komponente, umfassend ein Titanhalogenid oder -halogenalkoholat und gegebenenfalls einer Elektronendonorenbinding, getragen auf einem Magnesiumhalogenid in aktiver Form, wobei das Verfahren die folgenden Schritte umfaßt:
a) Vorkontakt der katalysatorbildenden Komponenten in weitgehender Abwesenheit von polymerisierbaren Olefinen (die Olefine sollten nicht in einer solchen Menge vorliegen, um mehr als 1 g
50 Polymer/g der Katalysatorkomponente zu erzeugen), um einen stereoselektiven Katalysator zu bilden, der in der Lage ist, während der Polymerisation des Gemisches von Propylen und α -Olefinen in Schritt c2) ein Copolymer mit einer Unlöslichkeit in Xylol bei 25 °C von mindestens 80 % zu ergeben;
b) Vorpolymerisation von Propylen oder Gemischen davon mit Ethylen und/oder α -Olefinen
55 $\text{CH}_2 = \text{CHR}$, worin R Alkyl mit 2 bis 10 Kohlenstoffatomen darstellt, unter Verwendung des in Schritt a) erhaltenen Katalysators, bei solchen Bedingungen, daß ein Polymer mit einer Unlöslichkeit in Xylol bei 25 °C von mehr als 60 %, in einer Menge von 1 bis 1000 g pro g fester Katalysatorkomponente erhalten wird;

c) Polymerisation der Monomere in der Gasphase, wobei in zwei oder mehreren in Reihe geschalteten Wirbelschicht- oder mechanisch gerührten Bettreaktoren gearbeitet wird, wobei ungeachtet der Reihenfolge:

- 5 c1) in einem der Reaktoren ein Gemisch von Ethylen und einem α -Olefin $\text{CH}_2 = \text{CHR}$, worin R einen Alkylrest mit 1 bis 10 Kohlenstoffatomen darstellt, zu einem Copolymer von Ethylen mit dem α -Olefin-Copolymer, das bis zu 20 Mol-% des α -Olefins enthält, polymerisiert wird; und
- 10 c2) in einem anderen Reaktor, nach Entfernen der nichtumgesetzten Monomere, die aus dem Reaktor c1) kommen, wenn c1) der erste Reaktor ist, ein Gemisch von Propylen und einem α -Olefin $\text{CH}_2 = \text{CHR}'$, worin R' einen Alkylrest mit 2 bis 10 Kohlenstoffatomen darstellt, zu einem Copolymer, das 5 bis 40 Gew.-% des α -Olefins in einer Menge von 5-30 Gew.-%, bezüglich des Gesamtgewichts des in c1) und c2) erhaltenen Polymers, enthält, polymerisiert wird;
- und wobei das Vorpolymerkatalysatorsystem, erhalten in b), in den Reaktor in c1) gespeist wird und das Polymerkatalysatorsystem, erhalten in c1), in den Reaktor in c2) gespeist wird, und wenn der erste Reaktor in c2) verwendet wird, die nichtumgesetzten Monomere, die aus c2) kommen, entfernt werden, bevor der Reaktor in c1) mit dem in c2) erhaltenen Polymerkatalysatorsystem gefüllt wird.
- 15 2. Verfahren nach Anspruch 1, wobei das in c2) gebildete Copolymer 10-15 Gew.-% des α -Olefins enthält und 15-25 % des Gesamtgewichts des in c1) und c2) erhaltenen Polymers bildet.
- 20 3. Verfahren nach den Ansprüchen 1 und 2, wobei das in c2) erhaltene Copolymer ein Propylen-Buten-Copolymer mit einer Unlöslichkeit in Xylol bei 25 °C von mehr als 85 % ist.
4. Verfahren nach Anspruch 1, wobei in Schritt c) zuerst das Propylen- α -Olefin- $\text{CH}_2 = \text{CHR}'$ -Gemisch von c2) polymerisiert wird und danach das Ethylen- α -Olefin-Gemisch von c1) polymerisiert wird.
- 25 5. Verfahren nach Anspruch 1, wobei der Katalysator durch Umsetzung einer Alkylaluminiumverbindung, einer Elektronendonoverbindung und der festen Komponente erhalten wird.
6. Verfahren nach Anspruch 5, wobei die Elektronendonoverbindung ein Silan der Formel $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ oder $\text{R}_1\text{Si}(\text{OR})_3$ darstellt, worin R_1 und R_2 , die gleich oder verschieden sind, Alkyl-, Cycloalkyl- oder Arylreste mit 1-18 Kohlenstoffatomen darstellen und R einen Alkylrest mit 1-6 Kohlenstoffatomen darstellt.
- 30 7. Verfahren nach Anspruch 1, wobei in den Reaktionsgasen ein Alkan mit 3-5 Kohlenstoffatomen in einer Konzentration von 20 bis 90 Mol-%, bezogen auf die Gesamtmenge an Gasen, gehalten wird.
- 35 8. Verfahren nach Anspruch 7, wobei das Alkan Propan ist.
9. Verfahren nach Anspruch 1, wobei die feste Katalysatorkomponente aus kugelförmig gestalteten Addukten von $\text{MgCl}_2 \cdot n\text{R}'\text{OH}$ erhalten wird, worin R' einen Alkyl- oder ein Cycloalkylrest mit 1-10 Kohlenstoffatomen darstellt und n eine Zahl von 3,5 bis 2,5 ist, wovon der Alkohol teilweise bis zu Werten für n von 2,5 bis 0,5 entfernt wird.
- 40 10. Ethylenpolymere in Form von Teilchen, wobei die Teilchen ein Gemisch eines linearen Copolymers von Ethylen mit einem α -Olefin $\text{CH}_2 = \text{CHR}$, worin R einen Alkylrest mit 1-10 Kohlenstoffatomen bedeutet, das bis zu 20 Mol-% des α -Olefins in einer Menge von 70 bis 95 Gew.-%, bezogen auf das Gesamtgewicht des Gemisches, enthält und eines Copolymers von Propylen mit einem α -Olefin $\text{CH}_2 = \text{CHR}'$, worin R' einen Alkylrest mit 2 bis 10 Kohlenstoffatomen bedeutet, das 5 bis 30 Gew.-% des α -Olefins in einer Menge von 5 bis 30 Gew.-%, bezogen auf das Gesamtgewicht des Gemisches, enthält, umfassen, wobei das Copolymer eine Unlöslichkeit in Xylol bei 25 °C von mindestens 80 % und eine Schmelzenthalpie von mehr als 70 J/g aufweist.
- 50 11. Pelletierte Massen, erhalten aus den Polymerteilchen, nach Anspruch 10.
- 55 12. Folien, erhältlich aus den Polymeren gemäß Ansprüchen 10 und 11.

Revendications

1. Procédé de préparation de polymères d'éthylène présentant une meilleure capacité de traitement par polymérisation d'éthylène avec des oléfines $\text{CH}_2 = \text{CHR}$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, à l'aide de catalyseurs comprenant le produit obtenu par réaction d'un dérivé alkyl-aluminium avec un constituant solide comprenant un halogénure de titane ou un halo-alcoolate et, éventuellement un dérivé d'électro-donneur supporté sur un halogénure de magnésium sous forme active, ledit procédé comprenant les étapes suivantes de:
 - a) pré-contact des constituants formant le catalyseur pratiquement en absence d'oléfines polymérisables (les oléfines ne doivent pas être présentes en quantité telle qu'il se forme plus d'1 g de polymère/g de composé catalytique) pour former un catalyseur stéréospécifique capable de donner au cours de la polymérisation du mélange de propylène et d'alpha-oléfines dans l'étape c2), un copolymère présentant une insolubilité dans le xylène à 25°C d'au moins 80%;
 - b) pré-polymérisation en utilisant le catalyseur obtenu dans l'étape a), de propylène ou de mélanges de propylène avec l'éthylène et/ou des alpha-oléfines $\text{CH}_2 = \text{CHR}$, où R est un radical alkyle comportant 2 à 10 atomes de carbone, dans des conditions telles que l'on obtient un polymère présentant une insolubilité dans le xylène à 25°C supérieure à 60%, en une quantité de 1 à 1000 g par g de constituant catalytique solide;
 - c) polymérisation des monomères en phase gazeuse, en opérant dans deux ou plus de deux réacteurs à lit fluidisé ou à lit agité mécaniquement connectés en séries, dans lesquels, dans un ordre quelconque, :
 - c1) dans l'un des réacteurs on polymérise un mélange d'éthylène et d'une alpha-oléfine $\text{CH}_2 = \text{CHR}$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, pour obtenir un copolymère d'éthylène avec ledit copolymère d'alpha-oléfine contenant jusqu'à 20% en moles d'alpha-oléfine; et
 - c2) dans un autre réacteur, après élimination des monomères n'ayant pas réagi provenant du réacteur c1), si c1) est le premier réacteur, on polymérise un mélange de propylène et d'une alpha-oléfine $\text{CH}_2 = \text{CHR}'$, où R' est un radical alkyle comportant 2 à 10 atomes de carbone, pour obtenir un copolymère contenant de 5 à 40% en poids de l'alpha-oléfine, en une quantité de 5 à 30% en poids par rapport au poids total du polymère obtenu en c1) et c2);
 et dans lequel le système prépolymère-catalyseur obtenu en b) est introduit dans le réacteur en c1) et le système polymère catalyseur obtenu en c1) est introduit dans le réacteur en c2), et dans le cas où le premier réacteur est utilisé en c2), les monomères n'ayant pas réagi provenant de c2) sont éliminés avant l'alimentation du réacteur en c1), avec le système polymère-catalyseur obtenu en c2).
2. Procédé selon la revendication 1 dans lequel le copolymère formé en c2) contient 10 à 15% en poids de l'alpha-oléfine et constitue 15 à 25% du poids total du polymère obtenu en c1) et c2).
3. Procédé selon les revendications 1 et 2, dans lequel le copolymère formé en c2) est un copolymère propylène-butène présentant une insolubilité dans le xylène à 25°C supérieure à 85%.
4. Procédé selon la revendication 1, dans lequel dans l'étape c) on polymérise d'abord le mélange propylène-alpha-oléfine $\text{CH}_2 = \text{CHR}'$ de c2) et ensuite on polymérise le mélange éthylène/alpha-oléfine de c1).
5. Procédé selon la revendication 1, dans lequel on obtient le catalyseur par réaction d'un dérivé alkyl-aluminium, d'un dérivé électro-donneur et du constituant solide.
6. Procédé selon la revendication 5, dans lequel le dérivé électro-donneur est un silane de formule $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ ou $\text{R}_1\text{Si}(\text{OR})_3$ dans lequel R_1 et R_2 , identique ou différent, sont des radicaux alkyle, cycloalkyle ou aryle comportant 1 à 18 atomes de carbone et R est un radical alkyle comportant 1 à 6 atomes de carbone.
7. Procédé selon la revendication 1, dans lequel, dans les gaz réactionnels, un alcane comportant 3 à 5 atomes de carbone est maintenu à une concentration comprise entre 20 et 90% en moles par rapport aux gaz totaux.
8. Procédé selon la revendication 7, dans lequel l'alcane est le propane.

9. Procédé selon la revendication 1, dans lequel le dérivé catalyseur solide est obtenu à partir de produits d'addition ou adducts sphérulisés $\text{MgCl}_2 \cdot n \text{ R}'\text{OH}$, où R' est un radical alkyle ou un radical cycloalkyle comportant de 1 à 10 atomes de carbone et n est un nombre entre 3,5 et 2,5, duquel l'alcool a été partiellement éliminé jusqu'à des valeurs de n comprises entre 2,5 et 0,5.

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10. Polymères d'éthylène sous forme de particules, lesdites particules comprenant un mélange d'un copolymère linéaire d'éthylène avec une alpha-oléfine $\text{CH}_2 = \text{CHR}$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, contenant jusqu'à 20% en moles de l'alpha-oléfine, en une quantité de 70 à 95% en poids par rapport au poids total du mélange, et un copolymère de propylène avec une alpha-oléfine $\text{CH}_2 = \text{CHR}'$, où R' est un radical alkyle comportant de 2 à 10 atomes de carbone, contenant de 5 à 30% en poids de l'alpha-oléfine, en une quantité de 5 à 30% en poids par rapport au poids total du mélange, ledit copolymère présentant une insolubilité dans le xylène à 25°C d'au moins 80% et une enthalpie de fusion supérieure à 70 J/g.

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11. Compositions granulées obtenues à partir de particules de polymère selon la revendication 10.

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12. Films obtenables à partir des polymères selon la revendication 10 et 11.

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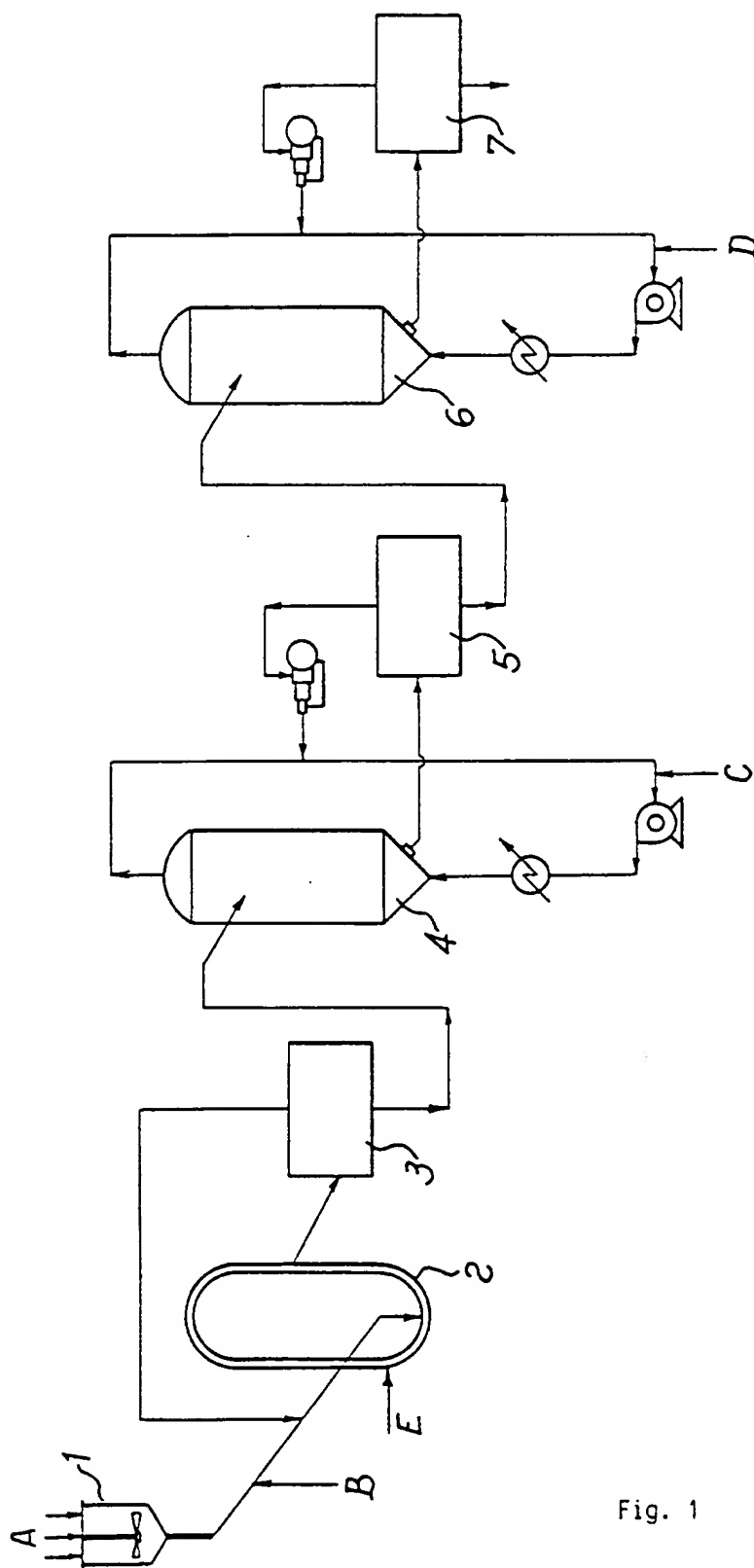
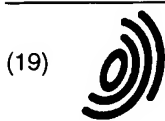


Fig. 1



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(54) **PROCESS FOR THE PREPARATION OF LINEAR LOW DENSITY POLYETHYLENE**

Verfahren zur Herstellung von linearen Polyäthylenen mit niedriger Dichte

PROCEDE DE PREPARATION DE POLYETHYLENE LINEAIRE DE FAIBLE DENSITE

- | | |
|---|---|
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Description

- [0001]** The present invention relates to a process for the preparation of linear low density polyethylene (LLDPE) endowed with improved processability by gas phase polymerization of the monomers, in two or more fluidized bed or mechanically stirred bed reactors, wherein, whatever the order, in one of the reactors mixtures of ethylene and an alpha-olefin $\text{CH}_2=\text{CHR}$ (R = alkyl having 1-10 carbon atoms) are polymerized to yield LLDPE and in another reactor mixtures of propylene and an alpha-olefin $\text{CH}_2=\text{CHR}'$, where R' is an alkyl radical having 2-18 carbon atoms, are polymerized, using the same catalyst in both reactors.
- [0002]** LLDPE has a variety of applications, but it is particularly employed in the preparation of films, because LLDPE films are endowed with improved mechanical and optical properties compared to films of LDPE.
- [0003]** The production of LLDPE films, however, shows some difficulties, mainly due to the fact that the polymer in the melted state has an insufficiently high melt strength, while its viscosity in the melted state is rather high.
- [0004]** In order to keep the productivity unaltered, it is necessary to modify the film extruders, for instance by widening the slit or increasing the temperature of the extruder head.
- [0005]** These modifications cause difficulties in the cooling of the bubble being blown at the extruder outlet and dishomogeneity in the film thickness.
- [0006]** In addition to these drawbacks, the hot welding of LLDPE films shows poor resistance to heat.
- [0007]** In order to overcome the shortcomings above, it was proposed to use blends of LLDPE with a semicrystalline copolymer of propylene with an alpha-olefin $\text{CH}_2=\text{CHR}'$ where R' is an alkyl radical having 2-10 carbon atoms, in particular 1-butene (U.S. Patent 4,871,813).
- [0008]** The copolymer contains from 7 to 40% by weight of alpha-olefin, has a fusion enthalpy lower than 75 J/g and is added in an amount of from 1 to 25% by weight.
- [0009]** The LLDPE-copolymer blend is prepared by mixing in the melted state the components pre-mixed in the solid state (in the form of powder or granules).
- [0010]** Mixing of the components in the solid state and feeding of such mixture directly into the extruder to mold the finished article is also contemplated.
- [0011]** The LLDPE is obtained by conventional polymerization methods, whereas the propylene-alpha olefin copolymer is prepared separately, employing stereospecific catalysts capable of yielding a semicrystalline copolymer having a fusion enthalpy not higher than 75 J/g.
- [0012]** The preparation of the above blends requires two separate polymerization lines for producing the two polymer components and then a blending step for mixing the components in the melt in an extruder. Blending of polymers in the melt is a high energy - consuming operation.
- [0013]** It has now been found that it is possible to produce blends of LLDPE and a propylene-alpha olefin $\text{CH}_2=\text{CHR}'$ copolymer endowed with improved processability and capable of forming films exhibiting good mechanical and optical properties directly in polymerization, using at least two reactors in series, wherein, whatever the order, in one of the reactors the LLDPE and in the other the propylene-alpha olefin copolymer are synthesized and wherein in both reactors the same catalyst is employed.
- [0014]** The use of the same catalyst in the various reactors in series has the advantage of utilizing a single production line instead of two, as well as growing the polymer blend onto each catalyst particle, thus obtaining a composition in which the components are homogeneously mixed in the solid state, with no need of the pelletization step which is necessary when the components are prepared by separate processes.
- [0015]** Therefore, the polymer can be directly fed into the film extruders, thereby attaining a higher film production rate and a lower energy consumption. In fact, the non-pelletized granules, not having been subjected to the melting-solidification process of the pelletization step, have lower crystallinity and higher melt index.
- [0016]** Moreover, the homogenization at the level of each single particle achievable by the process of the present invention has beneficial effects on the properties of the film.
- [0017]** The process of the invention comprises the following steps:
- a) pre-contact of the catalyst components in the substantial absence of polymerizable olefins (the olefins should not be present in such a quantity as to produce more than 1 g polymer/g of solid catalyst component) operating in such a way as to obtain a stereospecific catalyst capable of yielding during the polymerization step c2) a copolymer having an insolubility in xylene at 25°C of at least 80%;
 - b) pre-polymerization, using the catalyst obtained in step a), of propylene or mixtures thereof with ethylene and/or alpha-olefins $\text{CH}_2=\text{CHR}$, where R is an alkyl radical having from 2 to 10 carbon atoms, such as butene-1, hexene-1, 4-methyl-pentene-1, in such conditions as to obtain a polymer having an insolubility in xylene at 25°C higher than 60%, in an amount of from 1 to 1000 g per g of solid catalyst component;
 - c) polymerization of the monomers in gas phase, performed in two or more fluidized bed or mechanically stirred bed reactors in series, wherein, whatever the order:

c1) in one of the reactors a mixture of ethylene and an alpha-olefin $\text{CH}_2=\text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, is polymerized to obtain an ethylene-alpha olefin copolymer containing up to 20% by moles of alpha-olefin, and

5 c2) in another reactor, after removing the unreacted monomers coming from the reactor c1) if c1) is the first reactor, a mixture of propylene and an alpha-olefin $\text{CH}_2=\text{CHR}'$, where R' is an alkyl radical having from 2 to 10 carbon atoms, is polymerized to yield a copolymer containing from 5 to 40% by weight of the alpha olefin, in an amount of 5-30% by weight with respect to the total weight of the polymer obtained in c1) and c2);

10 and wherein the prepolymer-catalyst system obtained in b) is fed to the reactor in c1) and the polymer-catalyst system obtained in c1) to the reactor in c2). In case the first reactor is used in c2), the unreacted monomers coming from c2) are removed before feeding the reactor in c1) with the polymer-catalyst system obtained in c2).

[0018] Preferably, for an efficient control of the gas phase reaction, an alkane having 3-5 carbon atoms, preferably propane, is kept in the reaction gas, in particular in the first reactor where the catalyst reactivity is higher, in a concentration of from 20 to 90% by moles based on the total gas.

15 [0019] Preferably, the copolymer formed in c2) contains 10-15% by weight of the alpha-olefin and forms 15-25% of the total weight of the polymer in c1) and c2).

[0020] Surprisingly and unexpectedly the pre-forming of the catalyst, the pre-polymerization treatment with propylene and the presence of an alkane in the gas phase in the molar concentration indicated above, allow to control the polymerization process in the gas phase without the drawbacks usually encountered in the processes of the prior art, drawbacks which are essentially due to the low heat transfer capability of the gas phase and to the formation of electrostatic charges, which determine the tendency of the catalyst and the polymer particles to adhere to the reactor walls.

[0021] The catalyst employed in the process of the invention furthermore allows the polymer blend to grow onto each single particle of the solid catalyst component, so obtaining a good homogenization of the polymer blend.

[0022] The catalyst components employed in step a) comprise:

25 1) A solid component comprising a titanium compound containing at least one titanium-halogen bond supported on a magnesium halide in active form.

The solid component also contains an electron-donor compound (internal donor) when the catalyst itself is not sufficiently stereospecific for producing in step c2) propylene copolymers having the insolubility characteristics reported in c2).

30 As known, the stereospecificity of the catalysts supported on magnesium dihalide increases when using an internal donor.

As a general rule, the internal donor is always used in order to obtain catalysts capable of yielding in step c2) propylene-alpha olefin $\text{CH}_2=\text{CHR}'$ copolymers having an insolubility in xylene higher than 80% and preferably comprised between 85-94%.

35 2) An alkyl aluminum compound.

3) Optionally an electron-donor compound (external donor) of the same or of a different type with respect to the electron-donor present in the solid component 1).

40 The external donor is used to confer to the catalyst the required high stereospecificity. However, when particular diethers are employed as internal donors, such as those described in the European Patent Application A-344755, the catalyst stereospecificity is sufficiently high and no external donor is required.

[0023] The catalyst formed in step a) is fed continuously or discontinuously into step b).

45 [0024] Step b) can be carried out in liquid or gas phase. Preferably, step b) is carried out in the liquid phase, using as a liquid medium the propylene itself or a hydrocarbon solvent such as n-hexane, n-heptane, cyclohexane or an alkane having a low boiling point such as propane, butane (kept in the liquid state in the conditions employed in b).

[0025] The propylene pre-polymerization in step b) is carried out at a temperature comprised in the range of from 0° to 80°C, preferably from 5° to 50°C.

50 [0026] Propylene or the mixtures of propylene with ethylene and/or other alpha olefins, such as butene-1, hexene-1, 4-methyl pentene-1, are polymerized to yield polymers having an insolubility in xylene higher than 60%. The prepolymer yield ranges from 1 g to 1000 g of polymer per g of solid catalyst component, preferably from 5 g to 500 g of polymer per g of solid catalyst component.

[0027] Step b) can be performed continuously or discontinuously. In the former case, suitable means are employed for removing the unreacted propylene prior to feeding the prepolymer-catalyst system of step b) to the gas phase reactor.

[0028] The gas phase polymerization of step c) is performed according to known techniques operating in two or more fluidized bed or mechanically stirred bed reactors connected in series.

[0029] The monomers are fed into the two reactors in such a ratio as to yield a copolymer having the desired com-

position.

[0030] As indicated above, the unreacted monomers are removed prior to feeding the reaction mixture of the first reactor into the second reactor.

[0031] The process is carried out at a temperature lower than the syntherization temperature of the polymer. Generally the temperature is comprised between 50° and 120°C and preferably between 60° and 100°C. The total pressure is comprised between 1.5 and 3 MPa.

[0032] As indicated above, it is immaterial whether the ethylene-alpha olefin mixture is polymerized first to form the LLDPE copolymer or the propylene-alpha olefin $\text{CH}_2=\text{CHR}'$ mixture is polymerized first to form the corresponding copolymer.

[0033] However, synthesizing the propylene-alpha olefin copolymer in the first reactor is preferred, in order to obtain a polymer endowed with better flowability and a higher bulk density.

[0034] The propylene-alpha olefin copolymer is characterized by a fusion enthalpy (measure in accordance with the DSC method described in U.S. Patent 4,871,013) higher than 70 J/g, preferably comprised between 75 and 95 J/g, and by an isotactic index (determined by measuring the copolymer fraction which is insoluble in xylene at 25 °C) higher than 80 and generally comprised between 85 and 94.

[0035] Said DSC method consists in recording the enthalpy graph of a 5 mg sample of a copolymer by heating at a speed of 16°C. per minute up to 200°C., the sample having been previously subjected to a thermal treatment formed by heating at a speed of 16°C. per minute up to 200°C., followed by maintenance of such temperature for 20 minutes and cooling at a speed of 16°C. per minute down to 50°C.; the surface of the endothermic peak recorded during the heating is proportional to the melting enthalpy: the DSC analysis therefore enables the melting enthalpy of the copolymer to be measured, corresponding to the quantity required to melt 1 gramme of such copolymer.

[0036] Surprisingly, and in contrast with the characteristics of the propylene-alpha olefin copolymers used in the prior art, the process of the present invention allows to obtain LLDPE polymers endowed with good processability even though the crystallinity and isotacticity of the copolymer used are high.

[0037] As indicated above, the gas phase present in the various reactors preferably contains a $\text{C}_3\text{-C}_5$ alkane in a molar amount of from 20 to 90% with respect to the total gases. Examples of suitable alkanes are propane, butane, isobutane, n-pentane, isopentane, cyclopropane, cyclobutane. Propane is the preferred alkane.

[0038] The alkane is fed into the first reactor with the monomer mixture or separately and it is recycled with the recycle gas, i.e. with the portion of the gas which does not react in the bed and is removed from the polymerization zone, preferably by conveying it into a zone above the bed where the velocity is reduced and the particles entrained in the gas can again fall into the bed.

[0039] The recycle gas is then compressed and passed through a heat exchanger, where the heat of reaction is removed, before being recycled to the bed. See, for instance, U.S. Patents 3,298,792 and 4,518,750 for a description of the gas phase technology.

[0040] It is surprising and completely unexpected that the alkanes allow a very good control of the gas phase reaction whereas using an inert gas such as nitrogen is ineffective. In fact, the use of nitrogen does not prevent the formation of large polymer aggregates ("chunks"), which necessarily cause stopping of the operation of the plant.

[0041] According to a preferred embodiment, the alkane concentration in the first reactor is kept higher than that in the second (or subsequent) reactor.

[0042] Generally, the alkane is circulated through both reactors.

[0043] To achieve a complete fluidization, the recycle gas and, if preferred, a part or all of the make-up gas are reintroduced into the reactor at a point under the bed. A gas distribution plate, placed above the point of return, allows an effective distribution of the gas and furthermore acts as a support for the polymer bed when the gas flow is stopped.

[0044] Hydrogen can be used as chain transfer agent to control the molecular weight of the polymer.

[0045] A typical simplified scheme of the process is shown in the attached Figure 1. Reference numeral 1 indicates the apparatus where the catalyst components are pre-contacted. The loop reactor 2 is the pre-polymerization reactor. The gas phase reactors are indicated with 4 and 6, the solid-fluid separators with 3, 5 and 7. The catalyst components and the diluting agent (propane) are fed into the pre-contact reactor 1, as shown by arrows A. The pre-contacted catalyst is fed into the loop reactor 2 as shown by arrows B; propylene is fed into said loop reactor as shown by arrow E. The prepolymer-catalyst system is fed into the separator 3 and from the latter into the gas phase reactor 4, where, in the gas recycle line, propylene, the alpha olefin $\text{CH}_2=\text{CHR}'$, hydrogen and propane are fed, as shown by arrow C. The polymer which leaves the reactor 4, after passing through the separator 5, is introduced into the reactor 6, where ethylene, the alpha olefin $\text{CH}_2=\text{CHR}$, hydrogen and propane are fed, as shown by arrow D. The polymer in the form of spherical granules is discharged from the reactor 6 into the separator 7.

[0046] The active magnesium dihalides used as support for Ziegler-Natta catalysts are widely described in patent literature. The use of such dihalides is described for the first time in the U.S. Patents 4,298,718 and 4,495,338.

[0047] The magnesium dihalides which form the support for the catalyst components employed in the process of the present invention are characterized by X-ray spectra wherein the most intense diffraction line appearing in the spec-

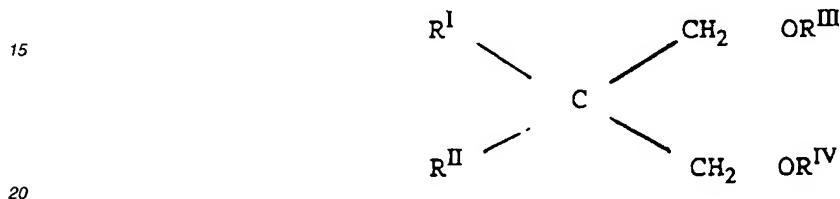
trum of the non-active halide has a lowered intensity and is substituted by a halo which maximum intensity is shifted toward lower angles with respect to the most intense line.

[0048] In the most active forms of the magnesium dihalides, the most intense line is no longer present and is substituted by a halo with the maximum intensity shifted as described above.

5 [0049] The titanium compounds suitable for the preparation of the solid catalyst component comprise the titanium halides, such as TiCl_4 , which is preferred, and TiCl_3 , and the haloalcoholates, such as trichlorophenoxy titanium and trichlorobutoxy titanium.

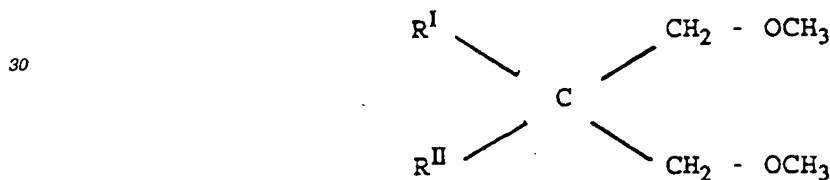
[0050] The titanium compound can be used as a mixture with other transition metal compounds, such as vanadium, zirconium and hafnium.

10 [0051] Suitable internal electron-donors comprise ethers, esters, amines, ketones and diethers of the general formula:



wherein R^{I} and R^{II} , equal to or different from each other, are alkyl, cycloalkyl and aryl radicals having from 1 to 18 carbon atoms, and R^{III} and R^{IV} , equal to or different from each other, are alkyl radicals having from 1 to 4 carbon atoms.

25 [0052] The preferred compounds are the alkyl, cycloalkyl and aryl esters of polycarboxylic acids such as phthalic and maleic acid and diethers of the formula:



wherein R^{I} and R^{II} are defined as above.

[0053] Examples of such compounds are: di-n-butyl-phthalate, di-isobutyl-phthalate, di-n-octyl-phthalate, 2-methyl-2-isopropyl-1,3-dimethoxy-propane, 2-methyl-2-isobutyl-1,3-dimethoxy-propane, 2,2-di-isobutyl-1,3-dimethoxypropane

40 and 2-isopropyl-2-isopentyl-1,3-dimethoxy-propane.

[0054] The internal donor is generally present in molar ratios of from 1:8 to 1:14 with respect to Mg. The titanium compound, expressed as Ti, is present in amounts of from 0.5 to 10% by weight.

[0055] The solid catalyst components can be prepared according to the methods described in the U.S. Patents 4,748,221 and 4,803,251.

45 [0056] If the stereospecificity of the obtained catalyst is insufficient for the purposes of the present invention, it can be easily modified according to the well known techniques described above.

[0057] Using the catalysts prepared from the catalyst components described in the European Patent Application EP-A-344,755, it is possible to obtain, with high specific activities (generally from 10 to 100 Kg/h/g of solid catalyst component), spherically shaped polymers with an average diameter of from 300 to 5000 μm (microns), endowed with high

50 bulk density and flowability.

[0058] In particular, in the European Application indicated above the catalyst components are prepared from spherulized adducts $\text{MgCl}_2 \cdot n \text{ROH}$ (R^{I} is an alkyl or cycloalkyl radical having 2-10 carbon atoms and n is a number from 3.5 to 2.5), from which the alcohol is partially removed by heating at increasing temperatures of from 50°C to 100°C.

[0059] In the formula above n is a number from 3.5 to 2.5; by heating, n is lowered to values of from 2.5 to 1 or lower.

55 [0060] The spherulized and partially de-alcoholated product is reacted with an excess of TiCl_4 at temperatures of from 80° to 135°C; the excess of TiCl_4 is removed for instance by hot filtration.

[0061] The treatment with TiCl_4 is usually repeated and the solid from which the unreacted TiCl_4 is removed is then washed with an inert hydrocarbon until the reaction of chlorine ions disappears.

[0062] The reaction with TiCl_4 is carried out in the presence of an electron-donor compound, selected in particular from the alkyl esters of the phthalic acid, such as di-n-butyl-phthalate, di-isobutyl-phthalate, di-n-octyl-phthalate, and the diethers having the general formula above.

[0063] The electron-donor compound can also be reacted with the adduct, before the reaction with the titanium compound.

[0064] The alkyl aluminum compound employed as co-catalyst is selected from the trialkyl aluminum compounds, such as Al-triethyl, Al-triisobutyl, Al-tri-n-butyl, Al-tri-n-octyl. Mixtures of trialkyl aluminum compounds with Al-alkylhalides or Al-alkyl-sesquihalides, such as AlEt_2Cl and $\text{Al}_2\text{Et}_3\text{Cl}_3$, can also be employed.

[0065] The Al/Ti ratio in the catalyst formed in step a) is greater than 1 and is generally comprised between 20 and 800.

[0066] The external donor can be the same or different from the electron-donor compound present as internal donor.

[0067] The molar ratio alkyl aluminum compound/external donor is generally comprised between 2 and 30.

[0068] When the internal donor is an ester of a polycarboxylic acid, particularly a phthalate, for instance isobutylphthalate or n-octylphthalate, the external donor is preferably selected from the silicon compounds of the formula $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ or $\text{R}_1\text{Si}(\text{OR})_3$, where R_1 and R_2 are alkyl, cycloalkyl or aryl radicals having from 1 to 18 carbon atoms and R is an alkyl radical having 1-6 carbon atoms. Examples of said silanes are methyl-cyclohexyl-dimethoxy silane, diphenyl-dimethoxy silane, methyl-t-butyl-dimethoxy silane and triphenyl methoxylane.

[0069] The diethers of the general formula reported above can also be conveniently used as external donors.

[0070] The solubility in xylene of the propylene polymer prepared in step b) and also of the propylene-alpha olefin copolymer is determined by dissolving 2 g of polymer in 250 ml of xylene at 135°C and stirring the system. After 20 minutes, the solution is cooled down to 25°C. After 30 minutes the precipitated material is filtered; the solution is evaporated in a nitrogen flow and the residue is dried at 80°C.

[0071] In this manner the percentage of polymer in xylene at room temperature and the percentage of insoluble polymer are calculated.

[0072] The following examples are given to better illustrate the invention and cannot be construed as limitative of its scope. Unless otherwise indicated, all the data are expressed by weight.

General procedure

[0073] The solid catalyst component employed in the examples is prepared as follows:

28.4 g of MgCl_2 , 49.5 g of anhydrous ethanol, 10 ml of vaseline oil ROL OB/30 and 100 ml of silicone oil having a viscosity of 350 cs are introduced, in an inert atmosphere, into a reactor equipped with a stirrer and heated to 120°C, until MgCl_2 is dissolved. The hot reaction mixture is then transferred into a 1,500 ml vessel, equipped with a stirrer Ultra Turrax T-45 N and containing 150 ml of vaseline oil and 150 ml of silicone oil. The temperature is kept at 120°C while stirring for 3 minutes at 3,000 r.p.m. The mixture is then discharged into a 2 liter vessel equipped with a stirrer and containing 1,000 ml of anhydrous n-heptane cooled to 0°C. The mixture is stirred at a speed of 6 meters per second for about 20 minutes, keeping the temperature at 0°C. The so obtained particles are recovered by filtration, washed with 500 ml of n-hexane and gradually heated, increasing the temperature from 50°C to 100°C for a time sufficient to reduce the alcohol content from 3 moles to the molar content indicated in the examples.

[0074] The adduct (25 g), containing the alcohol in the amounts indicated in the examples, is transferred into a reactor equipped with a stirrer and containing 625 ml of TiCl_4 at 0°C, under stirring. The reactor is then heated to 100°C for one hour. When the temperature is 40°C, di-isobutylphthalate is added in such an amount that the Mg/phthalate molar ratio is 8.

[0075] The reactor contents are then heated to 100°C for two hours and then the solid separates by sedimentation.

[0076] The hot liquid is removed by a siphon. 500 ml of TiCl_4 are added and the mixture is heated to 120°C for an hour under stirring. Stirring is stopped and the solid separates by sedimentation. The hot liquid is removed by a siphon. The solid is washed with portions of n-hexane at 60°C and then at room temperature.

Example 1.

[0077] An apparatus is utilized which operates in continuous and comprises a reactor in which the catalyst components are mixed to form the catalyst, a loop reactor receiving the catalyst formed in the previous step and being fed with liquid propylene and propane, and two fluidized bed reactors connected in series, the first reactor receiving the pre-polymer formed in the preceding step and discharging the polymer into the second reactor after removal of the unreacted monomers.

[0078] The process is carried out by feeding a solid catalyst component, prepared according to the general method reported above using a MgCl_2 /ethanol adduct containing 35% by weight of alcohol, a solution of triethyl aluminum (TEAL) in n-hexane and methyl-cyclohexyl-dimethoxysilane as electron-donor in such an amount that the TEAL/silane ratio is 4 by weight and the TEAL/Ti ratio is 120 by moles, into the pre-contact reactor kept at the constant temperature of 20°C. Into the same reactor propane is also fed as inert medium. The residence time is about 8.8 minutes.

[0079] The product discharged from the reactor is then fed into a loop pre-polymerization reactor kept at 50°C. The residence time in the loop reactor is about 80 minutes.

[0080] The first reactor receiving the pre-polymer produced in the preceding step operates at 60°C and at a reaction pressure of 1.8 MPa.

[0081] The average residence time of the polymer forming inside the reactor is about 80 minutes.

[0082] The reaction monomers and the gases fed into the reactor are the following:

- propylene and butene;
- hydrogen as molecular weight regulator;
- propane.

[0083] The first reactor discharges into a gas-solid separation system which removes the undesired monomer (propylene) before feeding the polymer to the second polymerization step.

20 Main operating conditions

Pre-contact step

[0084]

- temperature (°C)	= 20
- residence time (min.)	= 8.8

Pre-polymerization step

[0085]

- temperature (°C)	= 50
- residence time (min.)	= 80

First gas phase reactor

[0086]

- temperature (°C)	= 60
- pressure (MPa)	= 1.8
- residence time (min)	= 68
- propylene (mole%)	= 4.8
- butene-1 (mole%)	= 1.2
- hydrogen (mole%)	= 0.6
- propane (mole%)	= 89

(continued)

- % polymerization	= 11
- bonded butene (w%)	= 9.8
- MIL (230°C) (g/10 min)	= 21

Second gas phase reactor

[0087]

- temperature (°C)	= 90
- pressure (MPa)	= 1.75
- residence time (min)	= 76
- butene-1 (mole %)	= 8.6
- ethylene (mole %)	= 34
- hydrogen (mole %)	= 9.2
- propane (mole %)	= 44
- % polymerization	= 89
- bonded butene (wt %) (final)	= 7
- MIE (190°C, 2.16 Kg) (final) (g/10 min)	= 1.1
- F/E (21.6 Kg/2.16 Kg) (final)	= 35
- density (final) (g/cm ³)	= 0.916

Example 2

[0088] The same apparatus is used as in Example 1.

[0089] The process is carried out by feeding the catalyst components into the pre-contact reactor, kept at a constant temperature of 0°C with a residence time of 9.5 min.

[0090] The product discharged from the reactor is then fed into a loop pre-polymerization reactor, wherein a certain amount of liquid propylene and propane is also fed (as inert medium).

[0091] The residence time in the pre-polymerization reactor is about 80 minutes and the temperature is kept at 50°C.

[0092] The first reactor receiving the pre-polymer formed in the preceding step operates at 60°C and at a reaction pressure of 1.8 MPa.

[0093] The reaction monomers and the gases fed into the reactor are the following:

- ethylene;
- hydrogen as molecular weight regulator;
- propane.

Main operating conditions

Pre-contact step

5 [0094]

10

- temperature (°C)	= 0
- residence time (min)	= 9.5

Pre-polymerization step

15 [0095]

20

- temperature (°C)	= 50
- residence time (min)	= 80

First gas phase reactor

25 [0096]

30

35

40

- temperature (°C)	= 60
- pressure (MPa)	= 1.8
- residence time (min)	= 45
- propylene (mole %)	= 15
- butene-1 (mole %)	= 3.5
- hydrogen (mole %)	= 0.5
- propane (mole %)	= 80
- % polymerization	= 24
- bonded butene (wt %)	= 11.2
- MIL (230°C) (g/10 min)	= 6.1

45 Second gas phase reactor

[0097]

50

55

- temperature (°C)	= 90
- pressure (MPa)	= 1.75
- residence time (min)	= 83
- butene-1 (mole %)	= 4.8
- ethylene (mole %)	= 23

(continued)

- hydrogen (mole %)	= 4.2
- propane (mole %)	= 68
- % polymerization	= 76
- bonded butene (wt %) (final)	= 7.5
- MIE (190°C, 2.16 Kg) (final) (g/10 min)	= 1.14
- F/E (21.6/2.16) (final)	= 50
- density (final) (g/cc)	= 0.915

[0098] The particle size distribution of the polymers obtained in Examples 1 and 2 are reported in Table 1.

Table 1

		Example 1	Example 2
SIZE DISTRIBUTION	Units		
over 2,800 μm	wt %	0.5	1.0
over 2,000 μm	wt %	18.3	18.0
over 1,400 μm	wt %	45.0	41.6
over 1,000 μm	wt %	29.2	30.3
over 710 μm	wt %	5.0	7.5
over 500 μm	wt %	0.6	0.8
over 300 μm	wt %	0.3	0.4
over 180 μm	wt %	0.2	0.3
over 106 μm	wt %	0.1	0.1
Residue	wt %	---	---
BULK DENSITY			
Poured	g/cm^3	0.398	0.425
Tamped	g/cm^3	0.425	0.464
FLOWABILITY	s	10.0	9.0

Claims

1. Process for the preparation of ethylene polymers endowed with improved processability by polymerization of ethylene with olefins $\text{CH}_2 = \text{CHR}$, where R is an alkyl having 1-10 carbon atoms, by means of catalysts comprising the product obtained by reacting an alkyl aluminum compound with a solid component comprising a titanium halide or halo-alcoholate and optionally an electron-donor compound supported on a magnesium halide in active form, which process comprises the following steps:

- pre-contact of the catalyst-forming components in the substantial absence of polymerizable olefins (the olefins should not be present in such a quantity as to produce more than 1 g polymer/g of catalyst component) to form a stereospecific catalyst capable of yielding during the polymerization of the mixture of propylene and alpha olefins in step c2) a copolymer having an insolubility in xylene at 25° C of at least 80%;
- pre-polymerization, using the catalyst obtained in step a), of propylene or mixtures thereof with ethylene and/or alpha-olefins $\text{CH}_2 = \text{CHR}$, where R is an alkyl having from 2 to 10 carbon atoms, in such conditions as to obtain a polymer having an insolubility in xylene at 25°C higher than 60%, in an amount of from 1 to 1000 g per g of solid catalyst component;
- polymerization of the monomers in the gas phase, operating in two or more fluidized bed or mechanically

stirred bed reactors in series, wherein, whatever the order:

- 5 c1) in one of the reactors a mixture of ethylene and an alpha-olefin $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, is polymerized to obtain a copolymer of ethylene with said alpha olefin copolymer containing up to 20% by moles of the alpha-olefin; and,
 c2) in another reactor, after removing the unreacted monomers coming from the reactor c1) if c1) is the first reactor, a mixture of propylene and an alpha-olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having from 2 to 10 carbon atoms, is polymerized to yield a copolymer containing from 5 to 40% by weight of the alpha olefin, in an amount of 5-30% by weight with respect to the total weight of the polymer obtained in
 10 c1) and c2);

and wherein the prepolymer-catalyst system obtained in b) is fed into the reactor in c1) and the polymer-catalyst system obtained in c1) is fed to the reactor in c2), and in case the first reactor is used in c2), the unreacted monomers coming from c2) are removed before feeding the reactor in c1) with the polymer catalyst system obtained in
 15 c2).

2. Process according to claim 1, wherein the copolymer formed in c2) contains 10-15% by weight of the alpha-olefin and forms 15-25% of the total weight of the polymer obtained in c1) and c2).
- 20 3. Process according to claims 1 and 2, wherein the copolymer formed in c2) is a propylene-butene copolymer having an insolubility in xylene at 25°C higher than 85%.
4. Process according to claim 1, wherein in step c) firstly the propylene-alpha olefin $\text{CH}_2 = \text{CHR}'$ mixture of c2) is polymerized and thereafter the ethylene-alpha olefin mixture of c1) is polymerized.
- 25 5. Process according to claim 1, wherein the catalyst is obtained by reaction of an alkyl aluminum compound, an electron-donor compound and the solid component.
6. Process according to claim 5, wherein the electron-donor compound is a silane of formula $\text{R}_7\text{R}_2\text{Si}(\text{OR})_2$ or $\text{R}_1\text{Si}(\text{OR})_3$ wherein R_1 and R_2 , the same or different, are alkyl, cycloalkyl or aryl radicals with 1-18 carbon atoms and R is an alkyl radical with 1-6 carbon atoms.
- 30 7. Process according to claim 1, wherein in the reaction gases an alkane having 3-5 carbon atoms is kept in a concentration of from 20 to 90% by moles on the total gases.
8. Process according to claim 7, wherein the alkane is propane.
9. Process according to claim 1, wherein the solid catalyst component is obtained from spherulized adducts $\text{MgCl}_2 \cdot n \text{R}'\text{OH}$, where R' is an alkyl or a cycloalkyl radical having 1-10 carbon atoms and n is a number from 3.5 to 2.5, from which the alcohol is partially removed up to values for n of from 2.5 to 0.5.
- 40 10. Ethylene polymers in the form of particles, which particles comprise a mixture of a linear low density polyethylene formed of a copolymer of ethylene with an alpha olefin $\text{CH}_2 = \text{CHR}$, where R is an alkyl radical having from 1 to 10 carbon atoms, containing up to 20% by moles of the alpha olefin, in an amount of from 70 to 95% by weight with respect to the total weight of the mixture, and a copolymer of propylene with an alpha olefin $\text{CH}_2 = \text{CHR}'$, where R' is an alkyl radical having 2-10 carbon atoms, containing from 5 to 30% by weight of the alpha olefin, in an amount of from 5 to 30% by weight with respect to the total weight of the mixture, said copolymer having an insolubility in xylene at 25°C of at least 80% and a fusion enthalpy of more than 70 J/g.
- 50 11. Pelletized compositions obtained from the polymer particles according to claim 10.
12. Films obtainable from the polymers according to claims 10 and 11.

Patentansprüche

- 55 1. Verfahren zur Herstellung von mit verbesserter Verarbeitbarkeit ausgestatteten Ethylenpolymeren durch Polymerisation von Ethylen mit Olefinen $\text{CH}_2 = \text{CHR}$, worin R Alkyl mit 1-10 Kohlenstoffatomen darstellt, mit Hilfe von Katalysatoren, umfassend das Produkt, erhalten durch Umsetzen einer Alkylaluminiumverbindung mit einer festen

Komponente, umfassend ein Titanhalogenid oder -halogenalkoholat und gegebenenfalls einer Elektronendonatorverbindung, getragen auf einem Magnesiumhalogenid in aktiver Form, wobei das Verfahren die folgenden Schritte umfaßt:

- 5 a) Vorkontakt der katalysatorbildenden Komponenten in weitgehender Abwesenheit von polymerisierbaren Olefinen (die Olefine sollten nicht in einer solchen Menge vorliegen, um mehr als 1 g Polymer/g der Katalysatorkomponente zu erzeugen), um einen stereoselektiven Katalysator zu bilden, der in der Lage ist, während der Polymerisation des Gemisches von Propylen und α -Olefinen in Schritt c2) ein Copolymer mit einer Unlöslichkeit in Xylol bei 25°C von mindestens 80 % zu ergeben;
- 10 b) Vorpolymerisation von Propylen oder Gemischen davon mit Ethylen und/oder α -Olefinen $\text{CH}_2=\text{CHR}$, worin R Alkyl mit 2 bis 10 Kohlenstoffatomen darstellt, unter Verwendung des in Schritt a) erhaltenen Katalysators, bei solchen Bedingungen, daß ein Polymer mit einer Unlöslichkeit in Xylol bei 25°C von mehr als 60 %, in einer Menge von 1 bis 1000 g pro g fester Katalysatorkomponente erhalten wird;
- 15 c) Polymerisation der Monomere in der Gasphase, wobei in zwei oder mehreren in Reihe geschalteten Wirbelschicht- oder mechanisch gerührten Bettreaktoren gearbeitet wird, wobei ungeachtet der Reihenfolge:

c1) in einem der Reaktoren ein Gemisch von Ethylen und einem α -Olefin $\text{CH}_2=\text{CHR}$, worin R einen Alkylrest mit 1 bis 10 Kohlenstoffatomen darstellt, zu einem Copolymer von Ethylen mit dem α -Olefin-Copolymer, das bis zu 20 Mol-% des α -Olefins enthält, polymerisiert wird; und
20 c2) in einem anderen Reaktor, nach Entfernen der nichtumgesetzten Monomere, die aus dem Reaktor c1) kommen, wenn c1) der erste Reaktor ist, ein Gemisch von Propylen und einem α -Olefin $\text{CH}_2=\text{CHR}'$, worin R' einen Alkylrest mit 2 bis 10 Kohlenstoffatomen darstellt, zu einem Copolymer, das 5 bis 40 Gew.-% des α -Olefins in einer Menge von 5-30 Gew.-%, bezüglich des Gesamtgewichts des in c1) und c2) erhaltenen Polymers, enthält, polymerisiert wird;

25 und wobei das Vorpolymerkatalysatorsystem, erhalten in b), in den Reaktor in c1) gespeist wird und das Polymerkatalysatorsystem, erhalten in c1), in den Reaktor in c2) gespeist wird, und wenn der erste Reaktor in c2) verwendet wird, die nichtumgesetzten Monomere, die aus c2) kommen, entfernt werden, bevor der Reaktor in c1) mit dem in c2) erhaltenen Polymerkatalysatorsystem gefüllt wird.
- 30 2. Verfahren nach Anspruch 1, wobei das in c2) gebildete Copolymer 10-15 Gew.-% des α -Olefins enthält und 15-25 % des Gesamtgewichts des in c1) und c2) erhaltenen Polymers bildet.
- 35 3. Verfahren nach den Ansprüchen 1 und 2, wobei das in c2) erhaltene Copolymer ein Propylen-Buten-Copolymer mit einer Unlöslichkeit in Xylol bei 25°C von mehr als 85 % ist.
4. Verfahren nach Anspruch 1, wobei in Schritt c) zuerst das Propylen- α -Olefin- $\text{CH}_2=\text{CHR}'$ -Gemisch von c2) polymerisiert wird und danach das Ethylen- α -Olefin-Gemisch von c1) polymerisiert wird.
- 40 5. Verfahren nach Anspruch 1, wobei der Katalysator durch Umsetzung einer Alkylaluminiumverbindung, einer Elektronendonatorverbindung und der festen Komponente erhalten wird.
6. Verfahren nach Anspruch 5, wobei die Elektronendonatorverbindung ein Silan der Formel $\text{R}_1\text{R}_2\text{Si}(\text{OR})_2$ oder $\text{R}_1\text{Si}(\text{OR})_3$ darstellt, worin R_1 und R_2 , die gleich oder verschieden sind, Alkyl, Cycloalkyl- oder Arylreste mit 1-18 Kohlenstoffatomen darstellen und R einen Alkylrest mit 1-6 Kohlenstoffatomen darstellt.
- 45 7. Verfahren nach Anspruch 1, wobei in den Reaktionsgasen ein Alkan mit 3-5 Kohlenstoffatomen in einer Konzentration von 20 bis 90 Mol-%, bezogen auf die Gesamtmenge an Gasen, gehalten wird.
- 50 8. Verfahren nach Anspruch 7, wobei das Alkan Propan ist.
9. Verfahren nach Anspruch 1, wobei die feste Katalysatorkomponente aus kugelförmig gestalteten Addukten von $\text{MgCl}_2 \cdot n\text{R}'\text{OH}$ erhalten wird, worin R' einen Alkyl- oder ein Cycloalkylrest mit 1-10 Kohlenstoffatomen darstellt und n eine Zahl von 3,5 bis 2,5 ist, wovon der Alkohol teilweise bis zu Werten für n von 2,5 bis 0,5 entfernt wird.
- 55 10. Ethylenpolymere in Form von Teilchen, wobei die Teilchen ein Gemisch eines Polyethylens niedriger Dichte, gebildet aus einem linearen Copolymer von Ethylen mit einem α -Olefin $\text{CH}_2=\text{CHR}$, worin R einen Alkylrest mit 1-10 Kohlenstoffatomen bedeutet, das bis zu 20 Mol-% des α -Olefins in einer Menge von 70 bis 95 Gew.-%, bezogen

auf das Gesamtgewicht des Gemisches, enthält und eines Copolymers von Propylen mit einem α -Olefin $\text{CH}_2=\text{CHR}'$, worin R' einen Alkylrest mit 2 bis 10 Kohlenstoffatomen bedeutet, das 5 bis 30 Gew.-% des α -Olefins in einer Menge von 5 bis 30 Gew.-%, bezogen auf das Gesamtgewicht des Gemisches, enthält, umfassen, wobei das Copolymer eine Unlöslichkeit in Xylol bei 25°C von mindestens 80 % und eine Schmelzenthalpie von mehr als 70 J/g aufweist.

11. Pelletierte Massen, erhalten aus den Polymerteilchen, nach Anspruch 10.

12. Folien, erhältlich aus den Polymeren gemäß Ansprüchen 10 und 11.

Revendications

1. Procédé de préparation de polymères d'éthylène, présentant une meilleure aptitude au traitement, par polymérisation d'éthylène avec des oléfines $\text{CH}_2=\text{CHR}$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, à l'aide de catalyseurs comprenant le produit obtenu par réaction d'un dérivé alkyl-aluminium avec un constituant solide comprenant un halogénure de titane ou un halo-alcoolate et, éventuellement un dérivé électro-donneur supporté sur un halogénure de magnésium sous forme active ledit procédé comprenant les étapes suivantes de :

a) pré-contact des constituants formant le catalyseur pratiquement en absence d'oléfines polymérisables (les oléfines ne doivent pas être présentes en quantité telle qu'il se forme plus de 1g de polymère/g de composé catalytique) pour former un catalyseur stéréospécifique capable de donner au cours de la polymérisation du mélange de propylène et d' α -oléfines dans l'étape c2), un copolymère présentant une insolubilité dans le xylène à 25°C d'au moins 80 % ;

b) pré-polymérisation en utilisant le catalyseur obtenu dans l'étape a), de propylène ou de mélanges de propylène avec l'éthylène et/ou des α -oléfines $\text{CH}_2=\text{CHR}$, où R est un radical alkyle comportant 2 à 10 atomes de carbone, dans des conditions telles que l'on obtienne un polymère présentant une insolubilité dans le xylène à 25°C supérieure à 60°C, en une quantité de 1 à 1000 g par g de constituant catalytique solide :

c) polymérisation des monomères en phase gazeuse, en opérant dans deux ou plus de deux réacteurs à lit fluidisé ou à lit agité mécaniquement, connectés en séries, dans lesquels, dans un ordre quelconque :

c1) dans l'un des réacteurs, on polymérise un mélange d'éthylène et d'une α -oléfine $\text{CH}_2=\text{CHR}$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, pour obtenir un copolymère d'éthylène avec ledit copolymère d' α -oléfine contenant jusqu'à 20% en moles d' α -oléfine ; et

c2) dans un autre réacteur, après élimination des monomères n'ayant pas réagi provenant du réacteur c1, si c1) est le premier réacteur, on polymérise un mélange de propylène et d'une α -oléfine $\text{CH}_2=\text{CHR}'$, où R' est un radical alkyle comportant 2 à 10 atomes de carbone, pour obtenir un copolymère contenant de 5 à 40 % en poids de l' α -oléfine, en une quantité de 5 à 30 % en poids par rapport au poids total de polymère obtenu en c1) et c2) ;

et dans lequel le système prépolymère-catalyseur obtenu en b) est introduit dans le réacteur en c1) et le système polymère catalyseur obtenu en c1) est introduit dans le réacteur en c2), et dans le cas où le premier réacteur est utilisé en c2), les monomères n'ayant pas réagi provenant de c2) sont éliminés avant l'alimentation du réacteur en c1) avec le système polymère-catalyseur obtenu en c2).

2. Procédé selon la revendication 1, dans lequel le copolymère formé en c2) contient 10 à 15 % en poids de l' α -oléfine et constitue 15 à 25 % du poids total du polymère obtenu en c1) et c2).

3. Procédé selon les revendications 1 et 2, dans lequel le copolymère formé en c2) est un copolymère propylène-butène présentant une insolubilité dans le xylène à 25°C supérieure à 85 %.

4. Procédé selon la revendication 1, dans lequel dans l'étape c), on polymérise d'abord le mélange propylène/ α -oléfine $\text{CH}_2=\text{CHR}'$ de c2) et ensuite on polymérise le mélange éthylène/ α -oléfine de c1).

5. Procédé selon la revendication 1, dans lequel on obtient le catalyseur par réaction d'un dérivé alkyl-aluminium, d'un dérivé électro-donneur et du constituant solide.

6. Procédé selon la revendication 5, dans lequel le dérivé électro-donneur est un silane de formule $R_1R_2Si(OR)_2$ ou $R_1Si(OR)_3$ dans lesquels R_1 et R_2 , identiques ou différents, sont des radicaux alkyle, cycloalkyle ou aryle comportant 1 à 18 atomes de carbone et R est un radical alkyle comportant 1 à 6 atomes de carbone.
- 5 7. Procédé selon la revendication 1, dans lequel, dans les gaz réactionnels, un alcane comportant 3 à 5 atomes de carbone est maintenu à une concentration comprise entre 20 et 90 % en moles par rapport aux gaz totaux.
8. Procédé selon la revendication 7, dans lequel l'alcane est le propane.
- 10 9. Procédé selon la revendication 1, dans lequel le dérivé catalyseur solide est obtenu à partir de produits d'addition ou adducts sphérulisés $MgCl_2 \cdot n R'OH$, où R' est un radical alkyle ou un radical cycloalkyle comportant de 1 à 10 atomes de carbone et n est un nombre de 3,5 à 2,5, dont l'alcool a été partiellement éliminé jusqu'à des valeurs de n comprises entre 2,5 et 0,5.
- 15 10. Polymères d'éthylène sous forme de particules, lesdites particules comprenant un mélange d'un polyéthylène basse densité formé d'un copolymère d'éthylène avec une alpha-oléfine $CH_2=CHR$, où R est un radical alkyle comportant de 1 à 10 atomes de carbone, contenant jusqu'à 20 % en moles de l'alpha-oléfine, en une quantité de 70 à 95 % en poids par rapport au poids total du mélange, et un copolymère de propylène avec une alpha-oléfine $CH_2=CHR'$, où R' est un radical alkyle comportant de 2 à 10 atomes de carbone, contenant de 5 à 30 % en poids de l'alpha-oléfine, en une quantité de 5 à 30 % en poids par rapport au poids total du mélange, ledit copolymère
- 20 de l'alpha-oléfine, en une quantité de 5 à 30 % en poids par rapport au poids total du mélange, ledit copolymère présentant une insolubilité dans le xylène à 25°C d'au moins 80 % et une enthalpie de fusion supérieure à 70 J/g.
11. Compositions granulées obtenues à partir de particules de polymère selon la revendication 10.
- 25 12. Films obtenables à partir des polymères selon les revendications 10 et 11.

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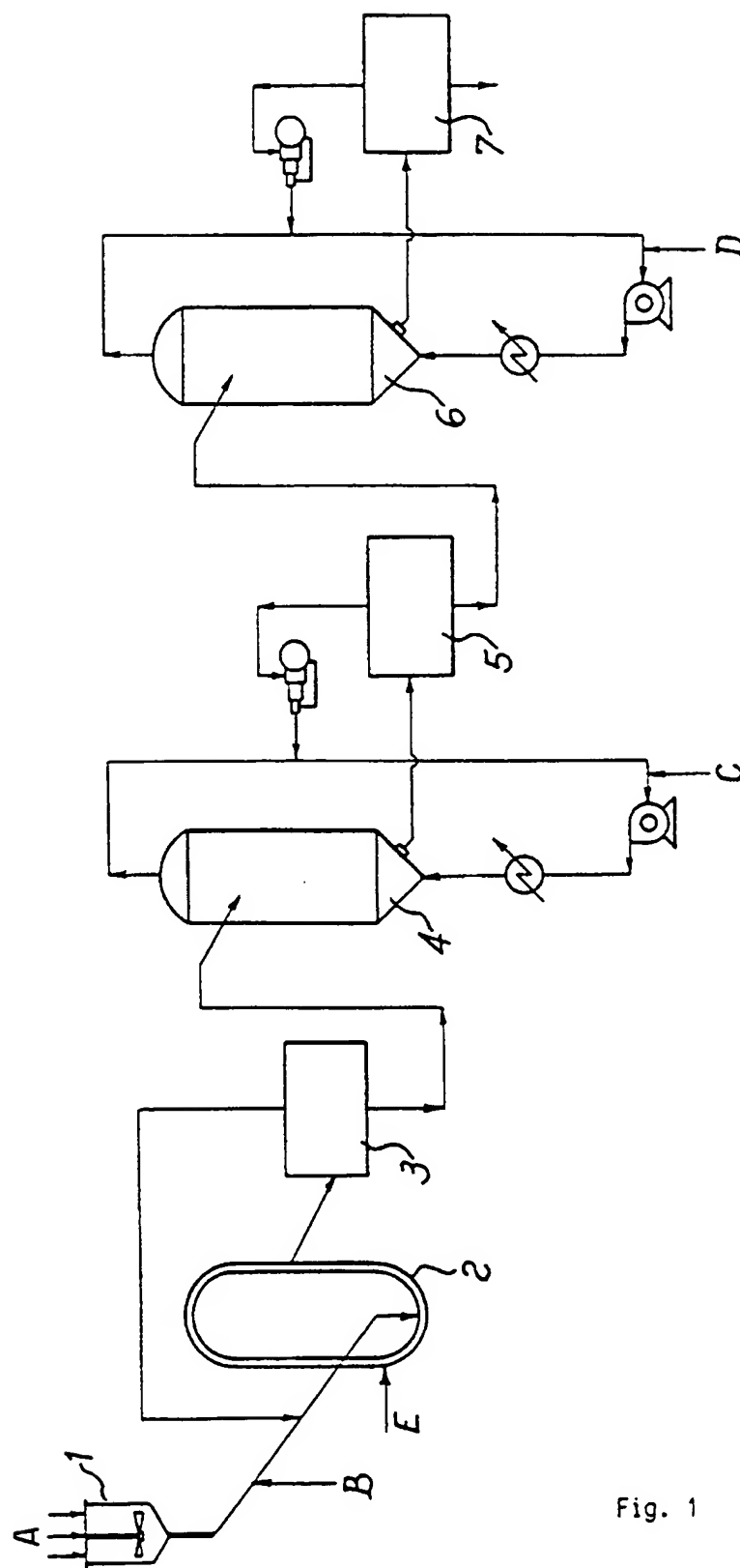


Fig. 1